

1. A spherical drop of liquid is suspended in an infinite atmosphere as shown in Fig-1. Owing to differences in temperature it is exchanging heat with its surroundings. It also is losing mass by evaporation to the surroundings. The instantaneous rate of heat transfer \dot{Q} is expressed by

$$\dot{Q} = KA(T - T_0)$$

where K is a constant and A is the surface area. The instantaneous rate of mass transfer is given by the symbol \dot{m} . It may be assumed that at a given instant of time the sphere is uniform in temperature and always at a pressure equal to that of the surroundings, P_0 . The vapor of the evaporating liquid in the region adjacent to the drop is saturated.

- (a) Derive an expression for the instantaneous time rate of change of the drop temperature, $\partial T / \partial t$ in terms of the significant physical quantities.
- (b) Estimate $\partial T / \partial t$ for water drop at $T_0 = 25^\circ\text{C}$, $P_0 = 2.339 \text{ Kpa}$, $T = 5^\circ\text{C}$, $r = 1 \text{ mm}$, $h_{fg} = 2489.6 \text{ KJ/Kg}$, $\dot{m} = 12.56 \times 10^{-3} \text{ g/min}$, $K = 6.0 \text{ KJ/m}^2 \text{ }^\circ\text{C}$, $c_p = 1.0 \text{ KJ/Kg }^\circ\text{C}$, $\rho = 1000 \text{ Kg/m}^3$.

2. It is proposed to build a one million kW electric power plant with steam as the working fluid. The condensers are to be cooled with river water (see Fig-2). The maximum steam temperature will be $T = 550^\circ\text{C}$ and the pressure in the condensers will be 10 kPa . and temperature $T_L = T_C = 45.8^\circ\text{C}$. As an engineering consultant, you are asked to estimate the resulting temperature rise ΔT of the river far downstream of the plant.

- (a) What is your estimate?
- (b) How the maximum stream temperature T_H affects the river tempere rise $\partial \Delta T / \partial T_H = ?$

3. Operation of an MHD converter requires an electrically conducting gas. It is proposed to utilize helium gas "seeded" with $y = 1.0$ mole percent cesium, as shown in Fig-3. The cesium is partly ionized ($\text{Cs} \rightleftharpoons \text{Cs}^+ + e^-$) by heating the mixture to 2500°K , 1 MPa in a nuclear reactor, in order to provide free electrons. No helium is ionized in this process, so that the mixture entering the converter consists of $\text{He}, \text{Cs}, \text{Cs}^+, e^-$. In order to analyze the converter process, it is necessary to know precisely the mole fraction of electrons in the mixture x .

- (a) Determine this seeded y cesiums affects the electrons in the mixture dx/dy . How
- (b) Determine this fraction x . At 2500°K , $\ln K = -13.4$ for the reaction given above.

4. Steam expands through a turbine in a cogeneration power cycle from 60 bars and 440°C to 0.08 bar . The turbine has an efficiency of 85 percent and delivers 50 MW of power. Steam is extracted at 5 bars for a heating load of $1 \times 10^6 \text{ kJ/min}$. The steam leaves the heating load as a saturated liquid at 4 bars mixes with the steam leaving the condensate pump at 4 bars (see Fig-4).

- (a) The pump efficiencies are both 70 percent. Sketch the diagram and explain how can you determine the following quantities: AS
- (b) The heat input in the boiler-superheater section,
- (c) The ratio of the heating load plus the turbine output to the heat input.

5. A thermoelectric generator such as show in Fig-5 converts heat directly to electrical energy without moving parts. Such a device has been proposed, for thermodynamic analysis, the power supply unit may be represented as shown in Fig-5.

Other data are as follows:

generator $\eta_{elec} = \frac{W_{elec}}{Q_H} = 0.15$

$\eta_{elec, motor} = 0.95$

Electric motor output = 2 kW

Fan requirement = 0.1 kW

Volumetric (dry) analysis of combustion products

		\bar{h}_f^o (kJ/kmol)	C_p (kJ/kmol K)
CO ₂	9.0%	-393522.	44.29
CO	1.0	-110529.	29.98
O ₂	7.0	0	31.17
N ₂	83.0	0	29.17
H ₂ O	?	-241827.	35.37

- (a) Write the combustion equation per mole of octane, and determine the percent theoretical air.
- (b) Calculate the octane flow rate.
- (c) Calculate the volume flow rate of cooling air required (inlet conditions).

$(\bar{h}_f^o, C_8H_{18} = -249952 \text{ kJ/k-mol})$

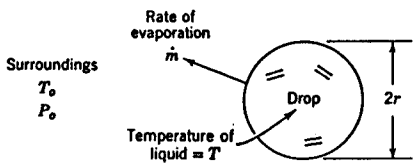


Fig-1

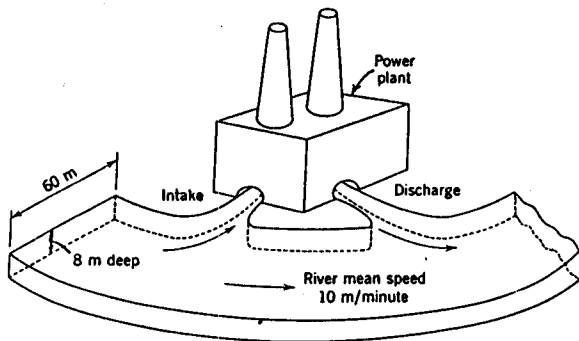


Fig-2

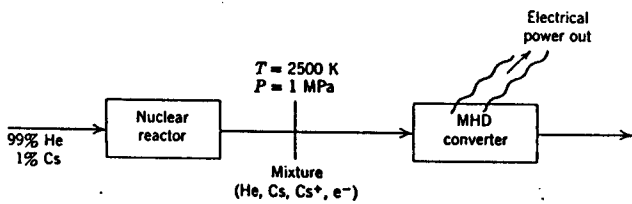


Fig-3

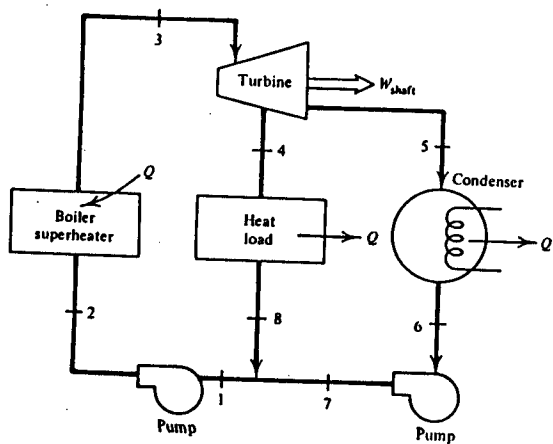


Fig-4

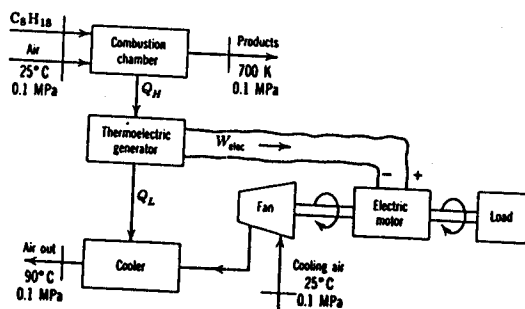


Fig-5