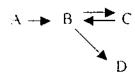
- 1. What is the meaning by "multiple steady states"? Please make a description for it. You have to specify the type of reactor which you are talking about. [6%]
- 2. Sketch the concentration profile of each component along a plug-flow reactor for the following reactions. All specific reaction rates are the same. [7%]



- 3. Reversible elementary reaction A_(g) ⇒ B_(g) is to be carried out in 640 °C. The feed is pure A at a total pressure of 3 atm and 640 °C. The feed rate is 4 gmole/min. The specific reaction rate of the forward reaction is 2 liter/gmole min and the concentration equilibrium constant is 0.3. [20%]
 - (a) Calculated the reactor volume necessary to achieve 95% of the equilibrium conversion of A in a plug-flow reactor.
 - (b) What will the volume change if the feed is diluted with other inert gas with when the other conditions remain unchanged? You should give your reason for this answer.
- 4. The following observations have been made about the reaction 2 GCH₃ → 2 GCH₂ + H₂
 - 1. The reaction rate is independent of hydrogen concentration.
 - 2. The reaction rate decreases with increasing concentrations of GCH₂.
 - 3. The initial rate appears to be first-order with respect to GCH3.
 - 4. When there is an extremely high concentration of GCH₂ and a low concentration of GCH₃, the reaction appears to be second-order with respect to GCH₃.
 - (a) Deduce a rate expression for the decomposition of GCH3. [5%]
 - (b) Suggest a mechanism and prove its correctness using pseudo-steady-state approximation. [10%]
- 5. A chemical reaction, its reaction rate at 227°C is 10 times of the rate at 127°C. Use Arrhenius' law to determine the activation energy of this reaction. (gas constant = 1.987 cal/mol K)[6%]
- 6. Assuming a stoichiometry A → R for a first-order gas reaction, we calculate the size of a mixed reactor needed for a given duty (90% conversion of a pure A feed) to be V = 32 liters. In fact, however, the reaction stoichiometry is A → 3 R. With this corrected stoichiometry, what is the required reactor volume? [13%]

7. Supported Rh catalysts have been employed to remove NO with CO addition:

$$CO + NO \xrightarrow{\text{th}} products(N_2, CO_2)$$

The mechanism is believed to be $CO + S \Leftrightarrow CO \bullet S$

$$NO + S \Leftrightarrow NO \bullet S$$

$$NO \bullet S + S \rightarrow N \bullet S + O \bullet S$$

$$CO \bullet S + O \bullet S \rightarrow CO_5 + 2S$$

$$N \bullet S + N \bullet S \rightarrow V_S + 2S$$

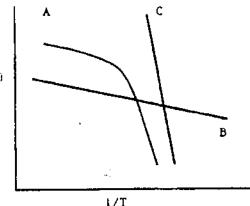
$$N \bullet S + N \bullet S \rightarrow N_S + 2S$$

When the ratio of P_{CO}/P_{NO} is small, show that the rate law is

$$-r_{CO} = \frac{kP_{CO}}{\left(1 + k_{CO}P_{CO}\right)^2}$$

[13%]

8. Curves A. B and C in Figure 1 show the variations in reaction rate for three different reactions catalyzed by solid catalyst pellets. What can you say about each reaction? [6%]



(a) Define the effectiveness factor and Thiele modulus. [6%]

(b) In the case of the reactions catalyzed by solids.

$$\phi = \frac{V}{S} \sqrt{\frac{n+1}{2} \frac{k(C_s^*)^{n-1} \rho_s}{D_{es}}} \quad nth - order \ irreversible \ reaction (n > -1)$$

$$\eta = \frac{1}{\phi} \left(\frac{3\phi \coth(3\phi) - 1}{3\phi} \right)$$

Figure 1

where ϕ : Thiele modulus.

 $E_{truc} = 2E_{app}$. [8%]

S. V: the external surface area and volume of the catalyst pellet.

k: reaction rate coefficient (mg³/kgcats).

 C_{i}^{*} : the concentration of the reactant on the external surface of the pellet.

 ρ_s : the density of the pellet.

Dea: internal diffusion constant.

n: effectiveness factor

Explain that for the internal diffusion control, the true reaction order is related to the measured reaction order by $n_{true} = 2n_{apparent} - 1$ and the true and apparent activation energies are related by