

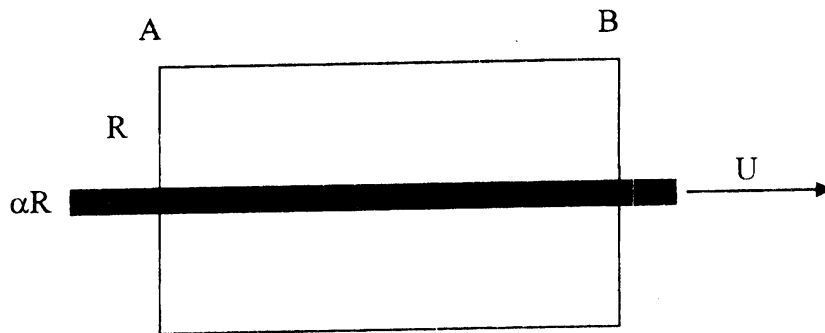
1. Consider an axial annular flow of a fluid confined between two cylinders as shown in the following figure. The inner cylinder with radius αR is moving to the right at velocity U while the outer cylinder with radius R is stationary. If ignoring the flow at both ends, the fluid flow is strictly axial laminar flow over most of the length L . Assuming the fluid is Newtonian and neglecting the gravity,

- (a) Please draw the velocity profile of the fluid flow between two cylinders. (3%)
- (b) Obtain the velocity profile of the fluid flow. (7%)
- (c) Derive the expression for the pressure difference between both ends. (5%)
(hint: begin with using the following dimensionless variables:

$$\frac{V_z(r)}{U} = v(s), \quad \frac{r}{R} = s, \quad \frac{\Delta P R^2}{4\mu L U} = \Psi(\alpha)$$

Which end has the higher pressure and how do you reach your answer? (2%)

- (d) If the viscosity of the fluid is 2 Poise, $L=25$ cm, $R=1$ cm, $\alpha=0.9$ and $U=1$ m/s, what is the pressure difference between both ends? (3%)



$$\rho \left(\frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta^2}{r} + v_z \frac{\partial v_r}{\partial z} \right) = -\frac{\partial P}{\partial r} + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r} (r v_r) \right) + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} + \frac{\partial^2 v_r}{\partial z^2} \right] + \rho g_r$$

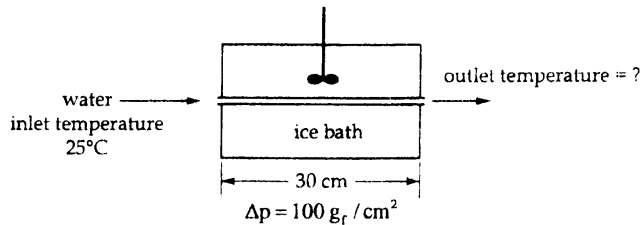
$$\rho \left(\frac{\partial v_\theta}{\partial t} + v_r \frac{\partial v_\theta}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_r v_\theta}{r} + v_z \frac{\partial v_\theta}{\partial z} \right) = -\frac{1}{r} \frac{\partial P}{\partial \theta} + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r} (r v_\theta) \right) + \frac{1}{r^2} \frac{\partial^2 v_\theta}{\partial \theta^2} + \frac{2}{r^2} \frac{\partial v_r}{\partial \theta} + \frac{\partial^2 v_\theta}{\partial z^2} \right] + \rho g_\theta$$

$$\rho \left(\frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right) = -\frac{\partial P}{\partial z} + \mu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_z}{\partial \theta^2} + \frac{\partial^2 v_z}{\partial z^2} \right] + \rho g_z$$

- 2. (a) What is the critical radius for insulation of cylinder or pipe? (5%)
- (b) The energy-transfer processes associated with the change in phase between a liquid and a vapor are more difficult to describe than the convective heat-transfer processes. Why? (6%)
- (c) Discuss the effect of liquid head and friction on capacity in tubular evaporators. (9%)

(背面仍有題目,請繼續作答)

3. Water is fed to a smooth capillary immersed in a well-stirred ice bath, as shown in the figure. The inlet temperature is 25°C and the wall temperature of the capillary is maintained at 0°C. The length (L) and inside diameter (D) of the capillary are 30 cm and 0.2 cm, respectively. In addition, the pressure drop across the capillary is 100 g_f/cm².



The properties of water are μ (viscosity) = 1 cp, C_p (heat capacity) = 4.184 J/g·K, k (thermal conductivity) = 0.570 W/m·K. Note that 1 cal = 4.184 J and 1 W = 1 J/sec.

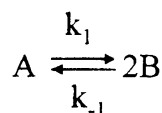
- (a) (7%) Estimate the average velocity of the flow if $f = 0.0791 Re^{-1/4}$ applies, where f is the friction factor and Re is the Reynolds number.
 (b) (5%) Estimate the logarithmic mean heat transfer coefficient h_{ln} if Colburn analogy applies, i.e., $j_{H,ln} = f/2$, where $j_{H,ln}$ is the Chilton-Colburn j -factor defined by

$$j_{H,ln} = \frac{Nu_{ln}}{Re Pr^{1/3}}$$

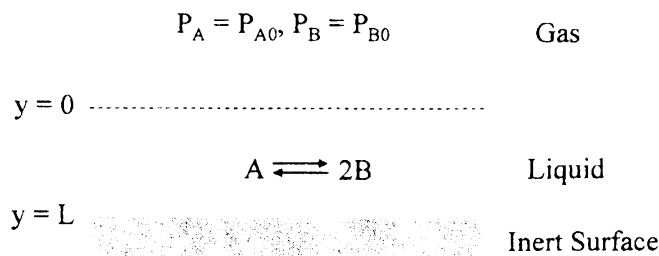
Here Pr is the Prandtl number and Nu_{ln} is the Nusselt number.

- (c) (8%) Estimate the outlet temperature from the capillary.

4. (20%) A gas mixture containing different partial pressure of species A (P_A) and B (P_B) dissolves in a stagnant liquid film as shown in the figure. The solubility of gas A and gas B in the liquid is α_A and α_B respectively. In the liquid, A is converted reversibly to B following first order chemical reaction. The reaction is



At steady state, determine the flux of A in the liquid film (assume that $D_A = D_B = D$).



本試題是否可以使用計算機： 可使用， 不可使用（請命題老師勾選）

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5. (a). A small water droplet evaporates in an air stream of temperature T and humidity \mathcal{H} . When a steady state is approached, before complete evaporation of this droplet, the temperature of the droplet is T_S . Please derive the following equation for obtaining the T_S : (make suitable assumption for your requirement) (12 %)

$$\frac{\mathcal{H} - \mathcal{H}_S}{T - T_S} = - \frac{h_y}{M_B k_y \lambda_S}$$

Where \mathcal{H} : the humidity of the air, M_B : molecular weight of air

\mathcal{H}_S : the saturation humidity at T_S ,

λ_S : latent heat of water at T_S ,

h_y and k_y : heat transfer and mass transfer coefficients, respectively, at gas/liquid interface

- (b). If the air temperature is 140 °F with a percentage humidity of 30%, determine the droplet temperature from the attached humidity chart. Please explain why this chart can be used and draw a simple figure to show how you find the answer from this chart? (4%)
- (c). If the air of problem (b) was fed into an adiabatic chamber containing sufficient amount of water droplets. In which, the humidity of the air was increased to a saturated condition. Please determine the temperature and humidity of the air leaving from the chamber. Describe how you obtain the answer (4%)

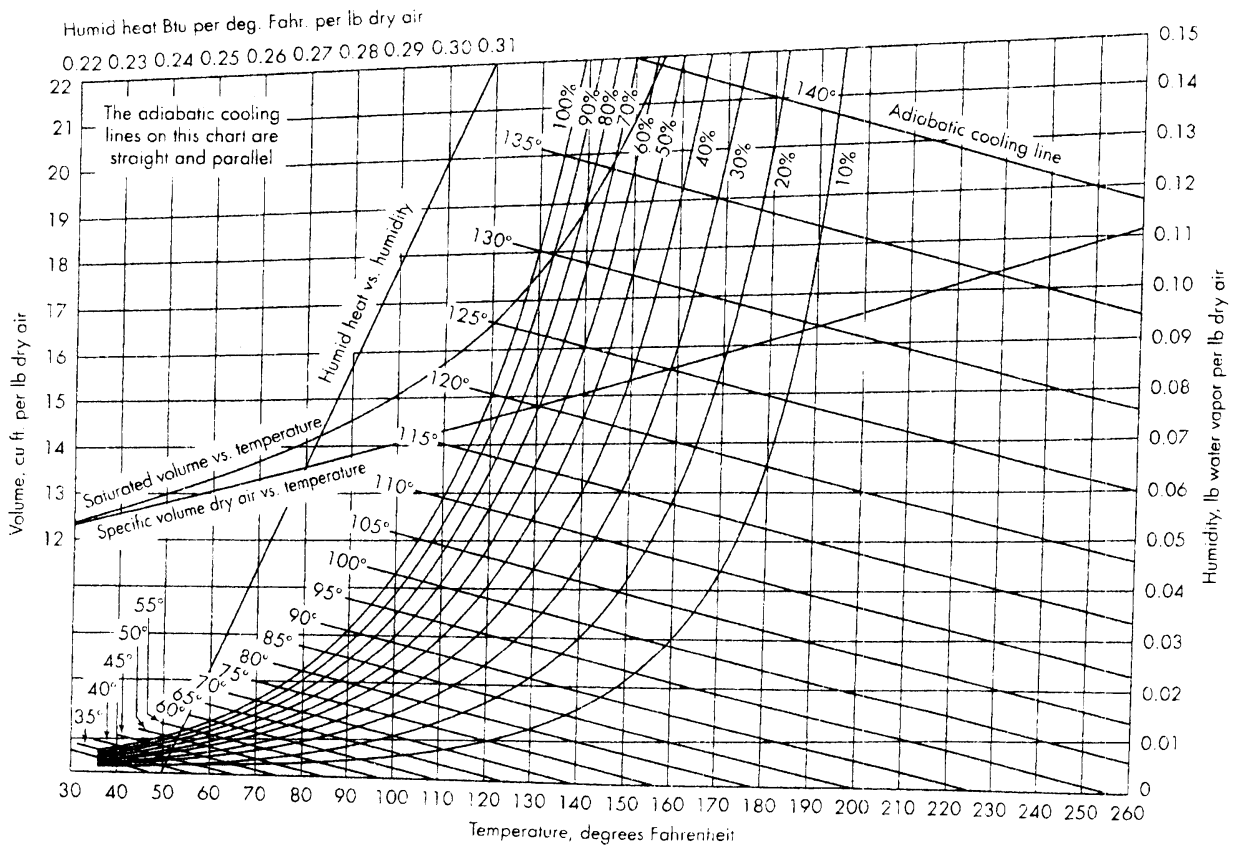


FIGURE
Humidity chart. Air-water at 1 atm.