1. Please show that the entropy of compressed liquid water is greater than the entropy of saturated liquid water for a temperature of 0°C, and is less than that of saturated liquid water for all the temperatures greater than 4°C. (10%)

2. Discuss the shape of the solid-liquid equilibrium curve on a P-T diagram for a substance that contracts on freezing in comparison with the curve for a substance that expands on freezing. (10%)

3. Initially a $0.05\ m^3$, insulated tank contains air at 20°C, 0.2 MPa. A valve is then opened and mass leaves the tank until the tank pressure reaches 0.10135 MPa. The valve is then closed. Determine
(a) the final temperature and the percentage of the mass left in the tank.
(b) the availability destruction and compare it to the initial availability of the system. (25%)
(The gas constant of air R is 0.287 KJ/kg°K)

4. Suppose that inlet temperatures to the compressor and the turbine are fixed for an air-standard Brayton cycle. Show that an expression for the maximum net work is

$$W_{max} = c_p T_1 \left(\sqrt{\frac{T_3}{T_1}} - 1\right)^2$$

Show that an expression for the pressure ratio that produces the maximum net work is

$$r_{p,opt} = \left(\frac{T_3}{T_1}\right)^{\frac{K}{2K-2}}$$

Note that 1 is the state at the inlet to the compressor, 3 is the state at the inlet to the turbine. (25%)

5. A hollow steel sphere having an inside diameter of 0.5 m and a 2-mm wall thickness contains water at 2 MPa, 250°C. This system (steel plus water) then cools to the ambient temperature, 30°C. Please write down the first and second law for this process. Determine if the process is reversible、irreversible or impossible. (30%)

Note: $C_p = 0.45\ KJ/Kg^{\circ}K$, $\rho = 7840\ Kg/m^3$ for steel
which C_p is specific heats and ρ is density.

Saturated Steam: Temperature Table

Temp. °C T	Press. kPa P	Specific Volume m³/kg Sat. Liquid v_f	Sat. Vapor v_g	Internal Energy kJ/kg Sat. Liquid u_f	Evap. u_{fg}	Sat. Vapor u_g	Enthalpy kJ/kg Sat. Liquid h_f	Evap. h_{fg}	Sat. Vapor h_g	Entropy kJ/kg K Sat. Liquid s_f	Evap. s_{fg}	Sat. Vapor s_g
0.01	0.6113	0.001 000	206.14	.00	2375.3	2375.3	.01	2501.3	2501.4	.0000	9.1562	9.1562
5	0.8721	0.001 000	147.12	20.97	2361.3	2382.3	20.98	2489.6	2510.6	.0761	8.9496	9.0257
10	1.2276	0.001 000	106.38	42.00	2347.2	2389.2	42.01	2477.7	2519.8	.1510	8.7498	8.9008
15	1.7051	0.001 001	77.93	62.99	2333.1	2396.1	62.99	2465.9	2528.9	.2245	8.5569	8.7814
20	2.339	0.001 002	57.79	83.95	2319.0	2402.9	83.96	2454.1	2538.1	.2966	8.3706	8.6672
25	3.169	0.001 003	43.36	104.88	2304.9	2409.8	104.89	2442.3	2547.2	.3674	8.1905	8.5580
30	4.246	0.001 004	32.89	125.78	2290.8	2416.6	125.79	2430.5	2556.3	.4369	8.0164	8.4533
35	5.628	0.001 006	25.22	146.67	2276.7	2423.4	146.68	2418.6	2565.3	.5053	7.8478	8.3531
40	7.384	0.001 008	19.52	167.56	2262.6	2430.1	167.57	2406.7	2574.3	.5725	7.6845	8.2570
215	2.104	0.001 181	0.094 79	918.14	1682.9	2601.1	920.62	1879.9	2800.5	2.4714	3.8507	6.3221
220	2.318	0.001 190	0.086 19	940.87	1661.5	2602.4	943.62	1858.5	2802.1	2.5178	3.7683	6.2861
225	2.548	0.001 199	0.078 49	963.73	1639.6	2603.3	966.78	1836.5	2803.3	2.5639	3.6863	6.2503
230	2.795	0.001 209	0.071 58	986.74	1617.2	2603.9	990.12	1813.8	2804.0	2.6099	3.6047	6.2146
235	3.060	0.001 219	0.065 37	1009.89	1594.2	2604.1	1013.62	1790.5	2804.2	2.6558	3.5233	6.1791
240	3.344	0.001 229	0.059 76	1033.21	1570.8	2604.0	1037.32	1766.5	2803.8	2.7015	3.4422	6.1437
245	3.648	0.001 240	0.054 71	1056.71	1546.7	2603.4	1061.23	1741.7	2803.0	2.7472	3.3612	6.1083
250	3.973	0.001 251	0.050 13	1080.39	1522.0	2602.4	1085.36	1716.2	2801.5	2.7927	3.2802	6.0730
255	4.319	0.001 263	0.045 98	1104.28	1496.7	2600.9	1109.73	1689.8	2799.5	2.8383	3.1992	6.0375
260	4.688	0.001 276	0.042 21	1128.39	1470.6	2599.0	1134.37	1662.5	2796.9	2.8838	3.1181	6.0019

Superheated Vapor

T	v	u	h	s	v	u	h	s	v	u	h	s
	P = 1.60 MPa (201.41)				P = 1.80 MPa (207.15)				P = 2.00 MPa (212.42)			
Sat.	.123 80	2596.0	2794.0	6.4218	.110 42	2598.4	2797.1	6.3794	.099 63	2600.3	2799.5	6.3409
225	.132 87	2644.7	2857.3	6.5518	.116 73	2636.6	2846.7	6.4808	.103 77	2628.3	2835.8	6.4147
250	.141 84	2692.3	2919.2	6.6732	.124 97	2686.0	2911.0	6.6066	.111 44	2679.6	2902.5	6.5453
300	.158 62	2781.1	3034.8	6.8844	.140 21	2776.9	3029.2	6.8226	.125 47	2772.6	3023.5	6.7664
350	.174 56	2866.1	3145.4	7.0694	.154 57	2863.0	3141.2	7.0100	.138 57	2859.8	3137.0	6.9563
400	.190 05	2950.1	3254.2	7.2374	.168 47	2947.7	3250.9	7.1794	.151 20	2945.2	3247.6	7.1271
500	.2203	3119.5	3472.0	7.5390	.195 50	3117.9	3469.8	7.4825	.175 68	3116.2	3467.6	7.4317
600	.2500	3293.3	3693.2	7.8080	.2220	3292.1	3691.7	7.7523	.199 60	3290.9	3690.1	7.7024
700	.2794	3472.7	3919.7	8.0535	.2482	3471.8	3918.5	7.9983	.2232	3470.9	3917.4	7.9487

(where T: °C; v: m³/Kg; u: KJ/Kg; h: KJ/Kg; S: KJ/Kg·K)