國立成功大學 106 學年度碩士班招生考試試題

系　所：機械工程學系

考試科目：熱力學

考試日期：0213，節次：2

※ 考生請注意：本試題可使用計算機。　請於答案卷(卡)作答，於本試題紙上作答者，不予計分。

1. (a) Consider a rigid tank divided by a partition into two equal compartments of volume V, each containing 1 mole of the same gas at the same temperature and pressure. Assume that the gas is ideal gas of constant heat capacity. Has any process taken place after the partition has been removed? If so, was it reversible or irreversible? Has any entropy change taken place? Explain.
   (b)A mass m of liquid at T_1 is isobarically and adiabatically mixed with an equal mass of liquid at T_2. Each mass is modeled as imcompressible with constant heat capacity c. Show that the entropy change of the entire system is

   $$\Delta S = 2mc\ \ln\left[\frac{T_1 + T_2}{2\sqrt{T_1 T_2}}\right]$$

   and $\Delta S > 0$. (30%)

2. Refrigerant 134a in a piston-cylinder assembly undergoes a process for which the pressure-volume relation is $pv^{1.05}$=constant. At the initial state, $v_1 = 0.09938\ \text{m}^3/\text{kg}$ and $P_1 = 200\ \text{kPa}$. The final temperature is $T_2 = 50\ °\text{C}$. Determine the final pressure, in kPa, using the table for the properties of superheated refrigerant 134a vapor on the next page. Evaluate the work for the process, in kJ/kg of refrigerant. (20%)

T °C	v m³/kg	u kJ/kg	h kJ/kg	s kJ/kg·K	v m³/kg	u kJ/kg	h kJ/kg	s kJ/kg·K
	p = 8.0 bar = 0.80 MPa (T_{sat} = 31.33°C)				p = 9.0 bar = 0.90 MPa (T_{sat} = 35.53°C)			
Sat.	0.02547	243.78	264.15	0.9066	0.02255	245.88	266.18	0.9054
40	0.02691	252.13	273.66	0.9374	0.02325	250.32	271.25	0.9217
50	0.02846	261.62	284.39	0.9711	0.02472	260.09	282.34	0.9566
60	0.02992	271.04	294.98	1.0034	0.02609	269.72	293.21	0.9897
70	0.03131	280.45	305.50	1.0345	0.02738	279.30	303.94	1.0214
80	0.03264	289.89	316.00	1.0647	0.02861	288.87	314.62	1.0521
90	0.03393	299.37	326.52	1.0940	0.02980	298.46	325.28	1.0819
100	0.03519	308.93	337.08	1.1227	0.03095	308.11	335.96	1.1109
110	0.03642	318.57	347.71	1.1508	0.03207	317.82	346.68	1.1392
120	0.03762	328.31	358.40	1.1784	0.03316	327.62	357.47	1.1670
130	0.03881	338.14	369.19	1.2055	0.03423	337.52	368.33	1.1943
140	0.03997	348.09	380.07	1.2321	0.03529	347.51	379.27	1.2211
150	0.04113	358.15	391.05	1.2584	0.03633	357.61	390.31	1.2475
160	0.04227	368.32	402.14	1.2843	0.03736	367.82	401.44	1.2735
170	0.04340	378.61	413.33	1.3098	0.03838	378.14	412.68	1.2992
180	0.04452	389.02	424.63	1.3351	0.03939	388.57	424.02	1.3245
	p = 10.0 bar = 1.00 MPa (T_{sat} = 39.39°C)				p = 12.0 bar = 1.20 MPa (T_{sat} = 46.32°C)			
Sat.	0.02020	247.77	267.97	0.9043	0.01663	251.03	270.99	0.9023
40	0.02029	248.39	268.68	0.9066				
50	0.02171	258.48	280.19	0.9428	0.01712	254.98	275.52	0.9164
60	0.02301	268.35	291.36	0.9768	0.01835	265.42	287.44	0.9527
70	0.02423	278.11	302.34	1.0093	0.01947	275.59	298.96	0.9868
80	0.02538	287.82	313.20	1.0405	0.02051	285.62	310.24	1.0192
90	0.02649	297.53	324.01	1.0707	0.02150	295.59	321.39	1.0503
100	0.02755	307.27	334.82	1.1000	0.02244	305.54	332.47	1.0804
110	0.02858	317.06	345.65	1.1286	0.02335	315.50	343.52	1.1096
120	0.02959	326.93	356.52	1.1567	0.02423	325.51	354.58	1.1381
130	0.03058	336.88	367.46	1.1841	0.02508	335.58	365.68	1.1660
140	0.03154	346.92	378.46	1.2111	0.02592	345.73	376.83	1.1933
150	0.03250	357.06	389.56	1.2376	0.02674	355.95	388.04	1.2201
160	0.03344	367.31	400.74	1.2638	0.02754	366.27	399.33	1.2465
170	0.03436	377.66	412.02	1.2895	0.02834	376.69	410.70	1.2724
180	0.03528	388.12	423.40	1.3149	0.02912	387.21	422.16	1.2980
	p = 14.0 bar = 1.40 MPa (T_{sat} = 52.43°C)				p = 16.0 bar = 1.60 MPa (T_{sat} = 57.92°C)			
Sat.	0.01405	253.74	273.40	0.9003	0.01208	256.00	275.33	0.8982
60	0.01495	262.17	283.10	0.9297	0.01233	258.48	278.20	0.9069
70	0.01603	272.87	295.31	0.9658	0.01340	269.89	291.33	0.9457
80	0.01701	283.29	307.10	0.9997	0.01435	280.78	303.74	0.9813
90	0.01792	293.55	318.63	1.0319	0.01521	291.39	315.72	1.0148
100	0.01878	303.73	330.02	1.0628	0.01601	301.84	327.46	1.0467
110	0.01960	313.88	341.32	1.0927	0.01677	312.20	339.04	1.0773
120	0.02039	324.05	352.59	1.1218	0.01750	322.53	350.53	1.1069
130	0.02115	334.25	363.86	1.1501	0.01820	332.87	361.99	1.1357
140	0.02189	344.50	375.15	1.1777	0.01887	343.24	373.44	1.1638
150	0.02262	354.82	386.49	1.2048	0.01953	353.66	384.91	1.1912
160	0.02333	365.22	397.89	1.2315	0.02017	364.15	396.43	1.2181
170	0.02403	375.71	409.36	1.2576	0.02080	374.71	407.99	1.2445
180	0.02472	386.29	420.90	1.2834	0.02142	385.35	419.62	1.2704
190	0.02541	396.96	432.53	1.3088	0.02203	396.08	431.33	1.2960
200	0.02608	407.73	444.24	1.3338	0.02263	406.90	443.11	1.3212

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3. A closed, rigid tank having a volume of 3 m^3 initially contains air at 100°C, 400 kPa, and 50% relative humidity. Assume the gas mixture act as an ideal gas, with Air: R = 0.287 kJ/kg-K; H_2O: R = 0.4615 kJ/kg-K. Properties are shown in the following tables. If the tank contents are cooled to 60°C, determine

(a) the temperature at which condensation begins, in °C. (5%)

(b) the mass of condensate, in kg. (5%)

(c) the heat transfer, in kJ. (10%)

(d) draw the process and locate the states on a T-v diagram. (5%)

Saturated Water		Specific volume, m^3/kg			Internal energy, kJ/kg		
Temp. (°C)	Press. (kPa)	Sat. Liquid v_f	Evap. v_{fg}	Sat. Vapor v_g	Sat. Liquid u_f	Evap. u_{fg}	Sat. Vapor u_g
50	12.350	0.001012	12.0308	12.0318	209.30	2234.17	2443.47
55	15.758	0.001015	9.56734	9.56835	230.19	2219.89	2450.08
60	19.941	0.001017	7.66969	7.67071	251.09	2205.54	2456.63
65	25.03	0.001020	6.19554	6.19656	272.00	2191.12	2463.12
70	31.19	0.001023	5.04114	5.04217	292.93	2176.62	2469.55
75	38.58	0.001026	4.13021	4.13123	313.87	2162.03	2475.91
80	47.39	0.001029	3.40612	3.40715	334.84	2147.36	2482.19
85	57.83	0.001032	2.82654	2.82757	355.82	2132.58	2488.40
90	70.14	0.001036	2.35953	2.36056	376.82	2117.70	2494.52
95	84.55	0.001040	1.98082	1.98186	397.86	2102.70	2500.56
100	101.3	0.001044	1.67185	1.67290	418.91	2087.58	2506.50

Ideal Gas Properties of Air

T (K)	h (kJ/kg)	u (kJ/kg)	s^o (kJ/kg K)
315	315.27	224.85	1.75106
320	320.29	228.42	1.76690
325	325.31	232.02	1.78249
330	330.34	235.61	1.79783
340	340.42	242.82	1.82790
350	350.49	250.02	1.85708
360	360.58	257.24	1.88543
370	370.67	264.46	1.91313
380	380.77	271.69	1.94001
390	390.88	278.93	1.96633
400	400.98	286.16	1.99194
410	411.12	293.43	2.01699
420	421.26	300.69	2.04142
430	431.43	307.99	2.06533
440	441.61	315.30	2.08870

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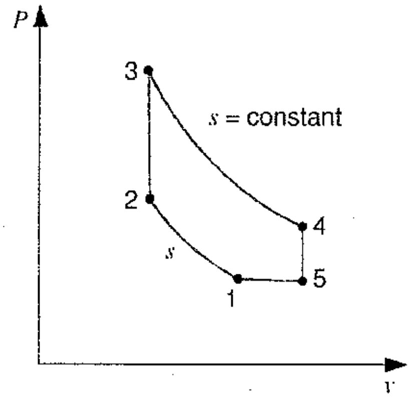
4. (15%) For an air-standard Miller cycle, P-v diagram is shown below. Assume air is an ideal gas with constant specific heats and specific heat ratio k. Please draw the cycle on a T-s diagram and show that its thermal efficiency is equal to $1-\dfrac{T_4-T_5}{T_3-T_2}-\dfrac{k(T_5-T_1)}{T_3-T_2}$



5. (10%) As known to all, ideal gas equation of state is $P=RT/v$ and C_p-C_v=R. Please find C_p-C_v for a gas which obeys the equation of state $P=RT/(v-b)$ where b is constant.