

系所組別： 奈米科技暨微系統工程研究所

考試科目： 熱力學

考試日期：0219，節次：1

※ 考生請注意：本試題 可 不可 使用計算機

1. A closed, rigid container with $V=0.5 \text{ m}^3$ has inside a liquid water vapor mixture at $p_1 = 1 \text{ bar}$ with a quality of 0.2. After heating for sufficient time, please determine if the final state could be a saturated vapor or saturated liquid. Please determine the amount of heat transfer required to reach the saturated state. (20%)
2. Assume that saturated steam at 1 bar in a pipe line is used to slowly feed into a closed, rigid and well insulated container with $V=0.5 \text{ m}^3$. The container is initially evacuated and is fed with steam until pressure inside reach 1 bar. Please determine the mass fed and the final temperature of the steam in the container. (20%)
3. Air enters an insulated compressor operating at steady state at 1 bar and 300°K with a mass flow rate of 1000 kg/h and exits at 8 bars. Please determine the minimum theoretical power input required and the exit temperature (the value of $k=c_p/c_v$ for air =1.4). (20%)
4. A rigid, well insulated tank is equally divided into two compartments that are separated by a valve. Initially, one of the compartments is evacuated and the other has 0.05 lb of air at 50 psi and 500°R . Please determine the final temperature and pressure if the valve is opened to allow air freely flows. Please also find the entropy production for the process. (Assume that air has $c_p=0.24$, $c_v=0.172 \text{ Btu/lb}^\circ\text{R}$ and the gas constant $R=0.06855 \text{ Btu/lb}^\circ\text{R}$) (20%)
5. Please explain the concept of exergy of a system, and how do you find exergy change for a close system when the system is undergoing a heat transfer and work done. (20%)

(背面仍有題目,請繼續作答)

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Table A-3 Properties of Saturated Water (Liquid-Vapor): Pressure Table

Pressure Conversions:
1 bar = 0.1 MPa
= 10² kPa

Press. bar	Temp. °C	Specific Volume m ³ /kg		Internal Energy kJ/kg		Enthalpy kJ/kg			Entropy kJ/kg · K		Press. bar
		Sat. Liquid v _f × 10 ³	Sat. Vapor v _g	Sat. Liquid u _f	Sat. Vapor u _g	Sat. Liquid h _f	Evap. h _{fg}	Sat. Vapor h _g	Sat. Liquid s _f	Sat. Vapor s _g	
0.04	28.96	1.0040	34.800	121.45	2415.2	121.46	2432.9	2554.4	0.4226	8.4746	0.04
0.06	36.16	1.0064	23.739	151.53	2425.0	151.53	2415.9	2567.4	0.5210	8.3304	0.06
0.08	41.51	1.0084	18.103	173.87	2432.2	173.88	2403.1	2577.0	0.5926	8.2287	0.08
0.10	45.81	1.0102	14.674	191.82	2437.9	191.83	2392.8	2584.7	0.6493	8.1502	0.10
0.20	60.06	1.0172	7.649	251.38	2456.7	251.40	2358.3	2609.7	0.8320	7.9085	0.20
0.30	69.10	1.0223	5.229	289.20	2468.4	289.23	2336.1	2625.3	0.9439	7.7686	0.30
0.40	75.87	1.0265	3.993	317.53	2477.0	317.58	2319.2	2636.8	1.0259	7.6700	0.40
0.50	81.33	1.0300	3.240	340.44	2483.9	340.49	2305.4	2645.9	1.0910	7.5939	0.50
0.60	85.94	1.0331	2.732	359.79	2489.6	359.86	2293.6	2653.5	1.1453	7.5320	0.60
0.70	89.95	1.0360	2.365	376.63	2494.5	376.70	2283.3	2660.0	1.1919	7.4797	0.70
0.80	93.50	1.0380	2.087	391.58	2498.8	391.66	2274.1	2665.8	1.2329	7.4346	0.80
0.90	96.71	1.0410	1.869	405.06	2502.6	405.15	2265.7	2670.9	1.2695	7.3949	0.90
1.00	99.63	1.0432	1.694	417.36	2506.1	417.46	2258.0	2675.5	1.3026	7.3594	1.00
1.50	111.4	1.0528	1.159	466.94	2519.7	467.11	2226.5	2693.6	1.4336	7.2233	1.50
2.00	120.2	1.0605	0.8857	504.49	2529.5	504.70	2201.9	2706.7	1.5301	7.1271	2.00
2.50	127.4	1.0672	0.7187	535.10	2537.2	535.37	2181.5	2716.9	1.6072	7.0527	2.50
3.00	133.6	1.0732	0.6058	561.15	2543.6	561.47	2163.8	2725.3	1.6718	6.9919	3.00
3.50	138.9	1.0786	0.5243	583.95	2546.9	584.33	2148.1	2732.4	1.7275	6.9405	3.50
4.00	143.6	1.0836	0.4625	604.31	2553.6	604.74	2133.8	2738.6	1.7766	6.8959	4.00
4.50	147.9	1.0882	0.4140	622.25	2557.6	623.25	2120.7	2743.9	1.8207	6.8565	4.50

Table A-4 Properties of Superheated Water Vapor

T °C	v m ³ /kg	u kJ/kg	h kJ/kg	s kJ/kg · K	v m ³ /kg	u kJ/kg	h kJ/kg	s kJ/kg · K
p = 0.70 bar = 0.07 MPa (T _{sat} = 89.95°C)					p = 1.0 bar = 0.10 MPa (T _{sat} = 99.63°C)			
Sat.	2.365	2494.5	2660.0	7.4797	1.694	2506.1	2675.5	7.3594
100	2.434	2509.7	2680.0	7.5341	1.696	2506.7	2676.2	7.3614
120	2.571	2539.7	2719.6	7.6375	1.793	2537.3	2716.6	7.4668
160	2.841	2599.4	2798.2	7.8279	1.984	2597.8	2796.2	7.6597
200	3.108	2659.1	2876.7	8.0012	2.172	2658.1	2875.3	7.8343
240	3.374	2719.3	2955.5	8.1611	2.359	2718.5	2954.5	7.9949
280	3.640	2780.2	3035.0	8.3162	2.546	2779.6	3034.2	8.1445
320	3.905	2842.0	3115.3	8.4504	2.732	2841.5	3114.6	8.2849
360	4.170	2904.6	3196.5	8.5828	2.917	2904.2	3195.9	8.4175
400	4.434	2968.2	3278.6	8.7086	3.103	2967.9	3278.2	8.5435
440	4.698	3032.9	3361.8	8.8286	3.288	3032.6	3361.4	8.6636
500	5.095	3131.8	3488.5	8.9991	3.565	3131.6	3488.1	8.8342